Report to

MID-AMERICA STEEL DRUM COMPANY, INC Oak Creek, WI Facility (FID 241021220)

for

PARTICULATE & VOC AIR EMISSIONS TESTING

of

DRUM RECLAMATION FURNACE (P30) & AFTERBURNER OPERATIONS (C30)

June 6, 2014



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DRUM RECLAMATION FURNACE (P30) & AFTERBURNER OPERATIONS (C30)

June 6, 2014

Michael J. Huenink Industrial Hygienist July 2, 2014

ENVIRONMENTAL TECHNOLOGY & ENGINEERING CORP 13000 W. Bluemound Road Elm Grove, Wisconsin 53122 Phone: (262) 784-2434 Fax: (262) 784 -2436

EXECUTIVE SUMMARY

On June 6, 2014, Environmental Technology & Engineering Corp (ETE) personnel visited the Mid-American Steel Drum Company facility (FID No. 241021220) located at 8570 South Chicago Road in Oak Creek, Wisconsin. The purpose of the visit was to perform air emissions testing on the Drum Reclamation Furnace Operation and its associated afterburner control device. This testing was requested by the Region 5 office of the US EPA in a letter dated March 5, 2014. Specifically, testing to determine total particulate emissions and the afterburner destruction efficiency of volatile organic compounds (VOCs) was requested. Testing was performed to address the EPA's request. The test results from this effort are compared to Wisconsin Department of Natural Resources (WDNR) Air Pollution Control Permit No. 241021220-P20 (P30, C30, S10), the document which includes the current emission limitations that have been assigned to these operations.

The results of the particulate testing indicated that the total particulate emissions were below (in compliance with) the WDNR permit limitations. The particulate test results can be summarized as follows:

Stack Tested	Test Date	Test	Total Particulate Emission Concentration	Total Particulate Emission Rate
		4		
S10 (Final Stack)	6/6	1	0.0087 gr/dscf	2.91 lb/hr
		2	0.0065 gr/dscf	2.11 lb/hr
		3	0.0057 gr/dscf	1.86 lb/hr
	s. 19 1	AVG	0.0070 gr/dscf	2.29 lb/hr
			The second secon	
WDNR Perm	it Limit	-		3.3 lb/hr

Notes: gr/dscf means grains of total particulate per dry standard cubic foot of exhaust gas lb/hr means pounds per hour

The results of the volatile organic compound (VOC) testing indicated that the VOC destruction efficiency of the afterburner was above (in compliance with) the WDNR permit limitations:

Stack Tested	Test Date	Test	VOC Concen. into Afterburner	VOC Concen. from Afterburner	VOC Destruction Efficiency
C30 (Afterburner)	6/6	1	32.2 mg/m3 (as C)	1.0 mg/m3 (as C)	96.95 %
		2	44.5 mg/m3 (as C)	0.5 mg/m3 (as C)	98.78 %
		3	36.5 mg/m3 (as C)	0.5 mg/m3 (as C)	98.54 %
		AVG			98.09 %
		2. (1.84)			
			WDNR Permit L	85 %	

Notes: mg/m3 (as C) means milligrams of total gaseous non-methane organics per dry standard cubic meter of exhaust gas, reported as carbon (as noted in EPA Method 25A)

1.0 GENERAL

On June 6, 2014, Environmental Technology & Engineering Corp (ETE) personnel visited the Mid-American Steel Drum Company facility (FID No. 241021220) located at 8570 South Chicago Road in Oak Creek, Wisconsin. The purpose of the visit was to perform air emissions testing on the Drum Reclamation Furnace Operation and its associated afterburner control device. This testing was requested by the Region 5 office of the US EPA in a letter dated March 5, 2014. Specifically, testing to determine total particulate emissions and the afterburner destruction efficiency of volatile organic compounds (VOCs) was requested.

The test efforts (and results included in this report) were performed to address the EPA's request. The test results are compared to Wisconsin Department of Natural Resources (WDNR) Air Pollution Control Permit No. 241021220-P20 (P30, C30, S10), the document which includes the current emission limitations that have been assigned to these operations:

Particulate matter (including condensables) - VOCs -

3.3 lb/hr

85% (or greater) control

The Mid-America Steel Drum Company (MASD) is involved in the reclamation and refurbishing of industrial steel drums. The operations (P30) targeted in this inquiry were the Drum Reclamation Furnace (Balboa Pacific), installed in 1995. The unit consists of a mechanical conveyor belt, combustion chamber and afterburner (C30). The combustion chamber and afterburner are both natural gas-fired. The combustion chamber is equipped with 12 burners, while the afterburner is equipped with 4 burners. The combined fuel burning capacity of the combustion chamber is 19.5 mmBtu/hr, while the combined fuel burning capacity of the afterburner is 6.5 mmBtu/hr. In addition to an afterburner, the entrance to the combustion chamber is equipped with a steam curtain. The exhaust ventilation system to the furnace is constructed so part of the exhaust stream, after the afterburner, can be diverted to a nearby boiler (Waste Heat Boiler). During the test efforts, the boiler was taken off-line (no exhaust gas was diverted to it) so that all of the afterburner exhaust was vented through the final stack (S10).

Drums are fed through the reclamation furnace "single file" at an average rate of 200 drums per hour. Since the amount of residual material in the drums varies, operators continually select the drums to be processed in order to achieve a relatively constant level of waste material through the process. During the test efforts, every effort was made to maintain a drum processing rate at, or above, the average drum processing rate. The drum counts during each test were as follows:

Test 1 - 247 drums per hour

Test 2 - 225 drums per hour

Test 3 - 255 drums per hour

1.0 GENERAL (continued)

The furnace was operated at an internal temperature of 1300-1400 °F, typical of normal operation. The afterburner was operated at a combustion zone setpoint of 1700 °F (permit requirements have the minimum setpoint limit of 1650 °F). A strip chart of the afterburner temperatures is included in Appendix A of this report.

Mr. Scott Swosinski of MASD and Ms. Amy Litscher of Saga Environmental & Engineering (environmental consultant) facilitated in the coordination of the production activities and field test efforts. Mr. Dakota Prentice of US EPA - Region 5, as well as Messrs. Michael Griffin and Ryan Bergh of the WDNR - Southeast Region received and reviewed the stack test notification protocol. The field test and analytical efforts were performed by ETE personnel; Michael Huenink was the test team leader.

2.0 RESULTS

2.1 Particulate Matter Results

Testing to determine particulate emissions was performed isokinetically using EPA Method 5 and 202 (back-half analysis procedures for condensable particulates). A brief description of the methodology is included in Section 3.1 of this report. A sketch showing the sampling port and point locations on the final discharge stack is included as Figure 2-1.

Three separate 60 minute tests were performed; the detailed total particulate emission results are included as Tables 2-1 through 2-3. The results of the particulate testing indicated that the total particulate emissions were below (in compliance with) the WDNR permit limitations. The particulate test results can be summarized as follows:

Stack Tested	Test Date	Test	Total Particulate Emission Concentration	Total Particulate Emission Rate
S10 (Final Stack)	6/6	1	0.0087 gr/dscf	2.91 lb/hr
		2	0.0065 gr/dscf	2.11 lb/hr
		3.	0.0057 gr/dscf	1.86 lb/hr
		AVG	0.0070 gr/dscf	2.29 lb/hr
WDNR Perm	it Limit	•		3.3 lb/hr

Notes: gr/dscf means grains of total particulate per dry standard cubic foot of exhaust gas lb/hr means pounds per hour

It might be noted that a larger probe sampling tip was utilized for the second and third tests, as compared to the first test. At the end of the first test, it was realized that a larger probe tip could be utilized in the testing, allowing for larger sample volumes. The decision was made to use a larger probe tip in order to minimize the impact of blank values and improve detection levels. All three tests had a sample volume greater than 30 cubic feet, meeting that criteria outlined in EPA Method 5.

2.2 VOC Results

Testing to determine VOC levels was performed using EPA Method 25A; a brief description of the methodology is included in Section 3.2 of this report. A sketch showing the sampling locations on the afterburner inlet duct and discharge end is included as Figure 2-2.

As noted in the test notification, the sampling locations immediately before and after the afterburner did not meet the EPA Method 2 criteria for proper location of air flow measurement (see attached sketch). Further, additional outside air is drawn into the final exhaust stack, following the afterburner, which would prevent that test location from being utilized for VOC destruction efficiency determination. For that reason, it was

2.2 VOC Results (continued)

proposed that the concentration of VOCs at each afterburner test location be used to determine the VOC destruction efficiency of the afterburner.

Static pressure measurements at the inlet and outlet of the drum reclamation furnace were made to verify that the operation remained negative to the outside air from a ventilation standpoint. Those readings indicated static pressures at the ends of the drum reclamation furnace that were 0.2 to 0.4 inches negative, relative to the outside air. Therefore, the capture efficiency of the furnace was assumed to be 100 percent and the control efficiency of the afterburner was then interpreted to be the same as the VOC destruction efficiency.

Testing was performed for three separate 60 minute test periods. The detailed results are included in Tables 2-4 through 2-6. The results of the VOC testing indicated that the VOC destruction efficiency of the afterburner was above (in compliance with) the WDNR permit limitations:

Stack Tested	Test Date	Test	VOC Concen. into Afterburner	VOC Concen. from Afterburner	VOC Destruction Efficiency
C30 (Afterburner)	6/6	1	32.2 mg/m3 (as C)	1.0 mg/m3 (as C)	96.95 %
		2	44.5 mg/m3 (as C)	0.5 mg/m3 (as C)	98.78 %
		3	36.5 mg/m3 (as C)	0.5 mg/m3 (as C)	98.54 %
		AVG			98.09 %
			85 %		

Notes: mg/m3 (as C) means milligrams of total gaseous non-methane organics per dry standard cubic meter of exhaust gas, reported as carbon (as noted in EPA Method 25A)

MID-AMERICA STEEL DRUM FINAL STACK S10 - DRUM RECLAMATION OPERATIONS

FIGURE 2-1

SAMPLE POINT LOCATIONS

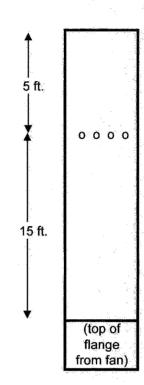
SAMPLE PORT LOCATION

Point	Distance from back wall (in.)
11-	4.5
2	13.5
3	22.5
4	31.5
5	40.5
6	49.5
	3.0
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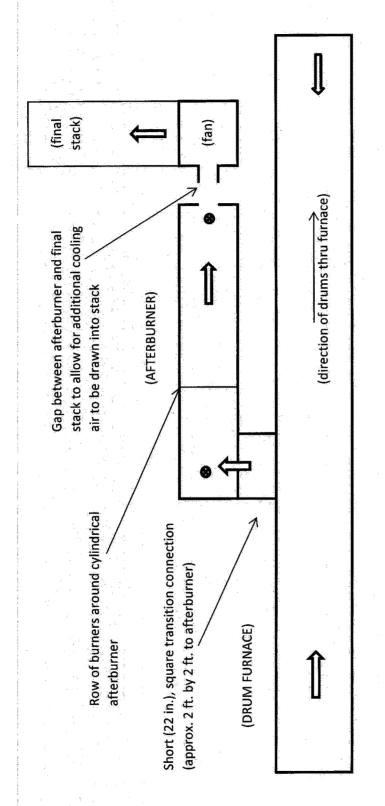
Stack Dimensions:

36 in. (wide) x 54 in. (deep)

Notes: 24 particulate sampling points on this rectangular stack; six points along each of four parallel traverses.



MID-AMERICA STEEL DRUM DRUM RECL. AFTERBURNER (C30) - SAMPLING LOCATIONS



(indicates the direction of air flow)

Proposed afterburner sampling locations for VOCs

TEST NO. 1	MID-AMERICA	STEEL DRUM	STACK S1	0	6/6/2014		TA	BLE 2-1
PAROMETRIC PRESSURE	TEOT NO		1					
TIP DIAMETER		DDESSIDE		IN HG				
STACK CDIMENSIONS 38								
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13 371 1.30 0.46 90 81.42 14 377 1.40 0.49 92 84.80 15 375 1.35 0.47 94 83.17 16 372 1.20 0.42 95 78.27 17 372 1.00 0.35 97 71.45 18 375 0.95 0.33 99 69.77 19 365 1.55 0.54 101 88.58 20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.10 0.39 106 74.49 24 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
14 377 1.40 0.49 92 84.80 15 375 1.35 0.47 94 83.17 16 372 1.20 0.42 95 78.27 17 372 1.00 0.35 97 71.45 18 375 0.95 0.33 99 69.77 19 365 1.55 0.54 101 88.58 20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 83.86 85CF PERCENT WATER VAPOR 93.86 65519 M3/HR PARTICULATE CONCENTRATION 9.0087 93.76 93.76 93.76 94.49 94.40		L						
16 372 1.20 0.42 95 78.27 17 372 1.00 0.35 97 71.45 18 375 0.95 0.33 99 69.77 19 365 1.55 0.54 101 88.58 20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 8559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017	14							
17 372 1.00 0.35 97 71.45 18 375 0.95 0.33 99 69.77 19 365 1.55 0.54 101 88.58 20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 0.5519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
18 375 0.95 0.33 99 69.77 19 365 1.55 0.54 101 88.58 20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								and the second s
19 365 1.55 0.54 101 88.58 20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
20 362 1.60 0.56 103 89.84 21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
21 360 1.35 0.47 104 82.42 22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION PARTICULATE EMISSION RATE PER 1000 LB GAS 2.91 LB/HR LB PART PER 1000 LB GAS 0.017		Walter State of the Control of the C						
22 361 1.25 0.44 105 79.36 23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								1 W 1
23 362 1.10 0.39 106 74.49 24 362 1.00 0.35 107 71.02 AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
AVERAGE 373 0.43 89 78.62 DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017		362						
DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017	24	362	1.00		0.35		107	71.02
DRY STANDARD VOLUME 33.86 SCF PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017	AVERAGE	373			0.43		89	78.62
PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017		₹ * [₹]			-		· 🕆 '	e de la companya de La companya de la co
PERCENT WATER VAPOR 2.18 % VOL FLOW RATE 63683 ACFM 38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
FLOW RATE		and the second s	7 (4) 5					***
38559 DSCFM 65519 M3/HR PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017		TER VAPOR						
65519 M3/HR	FLOW RATE	-						
PARTICULATE CONCENTRATION 0.0087 GR/DSCF PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017								
PARTICULATE EMISSION RATE 2.91 LB/HR LB PART PER 1000 LB GAS 0.017	PARTICUL AT	E CONCENTRATION			-			
LB PART PER 1000 LB GAS 0.017	the first office with report to the first of the							
	and the second s	The state of the s		en grand at t				
	A 2 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	원이 가장 그렇게 가장하지 않게 먹는 것이다.						

MID-AMERICA	STEEL DRUM		STACK S1	0	6/6/2014			TABLE	2-2
NUMBER OF I METER VOLU PITOT COEFF METER COEF PARTICULATI WATER COLL STATIC PRES	R NSIONS ME PER POINT POINTS ME TICIENT FICIENT E COLLECTED SURE		2 29.27 0.250 36 13.500 2.5 24 55.65 0.84 1.009 0.0235 16 -0.56	IN HG IN IN FT3 MIN FT3 GRAMS ML IN H2O	54	IN			
ORSAT RESU	LTS O2	O2		CO		N2			
	20%	19.20%		0.00%		79.60%		4	
TEST POINT	STACK TEMP DEG F		PITOT DEL P IN H2O		ORIFICE DEL P IN H2O		METER TEMP DEG F		STACK VELOCITY AFPS
1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20	360 360 359 358 358 357 360 361 362 363 362 359 355 352 352 353 351 350 350 352		1.40 1.40 1.30 1.15 1.05 0.95 1.55 1.35 1.30 1.15 1.00 0.95 1.45 1.30 1.20 1.05 0.95 1.25 1.35		1.40 1.40 1.30 1.15 1.05 0.95 1.55 1.35 1.30 1.15 1.00 0.95 1.45 1.30 1.20 1.05 1.05 0.95 1.35		100 101 103 105 106 107 109 109 110 111 112 113 115 116 117 118 119 121 122 123		83.84 83.84 80.74 75.90 72.52 68.94 88.22 82.38 80.89 76.13 70.95 69.02 85.07 80.40 77.24 72.30 72.21 68.64 81.83 78.84 77.34
21 22	354 355		1.20 1.10	-	1.20		123		77.34 74.09
23	354		1.00		1.00		124	1	70.60
24	351		0.90		0.90		124		66.85
AVERAGE	356				1.18		113		76.62
PARTICULATI	TER VAPOR CONCENTRAT EMISSION RAT	100	55.38 1.34 62059 38694 65749 0.0065 2.11 0.012 94.5	SCF % VOL ACFM DSCFM M3/HR GR/DSCF LB/HR					

MID-AMERICA	A STEEL DRUM		STACK S1	0	6/6/2014		•	TABLE 2-3
TECT NO			1					
TEST NO.	DDEOGUDE			IN LIG			+	
BAROMETRIC	4. The second of the second		29.27	IN HG				The second second
TIP DIAMETE	L "		0.250	IN	#5.A	INT		
STACK DIME	A Section of the sect		36	IN	54	IN		
STACK AREA			13.500	FT3				
and the second of the second o	ME PER POINT		2.5	MIN				
NUMBER OF			24					
METER VOLU			56.54	FT3				
PITOT COEFF	1 34 ST		0.84					
METER COEF			1.009	ing single and a large				* /
the state of the s	E COLLECTED		0.0208	GRAMS				and the state of
WATER COLL			18	ML				
STATIC PRES	SURE		-0.69	IN H2O				
00047.050								
ORSAT RESU	1	600		co		N2		
	20%	O2 19.20%		0.00%		79.60%		大手 海 医
l	20%	19.20%		0.00%		1 3.00 %		en e
TEST	STACK		PITOT		ORIFICE		METER	STACK
POINT	TEMP		DEL P		DEL P		TEMP	VELOCITY
POINT	DEG F		IN H2O		IN H2O		DEG F	AFPS
	DCO.		1141129		1141,20			
1	370		1.45		1.45		105	85.88
	367		1.40		1.40		105	84.20
3	366		1.30		1.30		106	81.09
2 3 4	365		1.20		1.20		108	77.86
5	362		1.10		1.10		108	74,41
6	360		1.00		1.00		109	70.86
6 7 8	362		1.55		1.55		110	88.33
8	363	*	1.45		1.45		111	85.48
9	361		1.30		1.30		112	80.84
10	360		1.20		1.20		114	77.62
11	360		1.10		1.10		116	74.32
12	360		0.95		0.95		116	69.07
13	360		1.45		1.45		116	85.33
14	363		1.30		1.30		117	80.94
15	365	s'	1.25		1.25		118	79.47
16	363		1.25		1.25		118	79.37
17	362		1.15		1.15		118	76.08
18	361		1.05		1.05		119	72.65
19	362		1.35		1.35		120	82.43
20	362		1.30		1.30		120	80.89
21	363		1.20		1.20		120	77.77
22	362		1.15		1.15		120	76.08
23	360		0.95		0.95		121	69.07
. 24	360	1.	0.85		0.85		121	65.33
AVEDAGE	200				4.00		445	70 44
AVERAGE	362				1.22		115	78.14
DRY STANDA	RD VOLUME		56.28	SCF			÷	
PERCENT WA			1.48	% VOL				
FLOW RATE	en transpiewe en Mytte		63294	ACFM			4	
	1. Administration of the Control of		39093	DSCFM				
			66427	M3/HR				
PARTICULATI	E CONCENTRATI	ON	0.0057	GR/DSCF	-			
and the second of the second o	E EMISSION RAT		1.86	LB/HR				
	1000 LB GAS		0.011				*	The second second
ISOKINETIC P			95.0					
	n de la fille de l							

VOCS - TEST 1 STACK S10 - DRUM RECLAM FURNACE & AFTERBURNER MID-AMERICA STEEL DRUM - OAK CREEK, WI TABLE 2-4

JUNE 6, 2014

INLET				OUTLE	r			
TIME	VOC TIME PPM	VOC PPM		TIME	VOC PPM	TIME	VOC PPM	
1	21.6 31	21		1	2.5	31	1.7	
	21.1 32	26.1		2	3.2	32	1.5	1 1 Table
3	20.8 33	32.9		3	2.4	33	1.5	- A
4	15.1 34	33.4		4	2.6	34	1.6	
5	11.5 35	42.4		5	3.5	35	1.6	18 6 6
2 3 4 5 6	11.6 36	39		6	3.4	36	1.5	
7	26.5 37	46.8		7	3.0	37	1.6	1
8	60.3 38	40.6		8	1.8	38	1.4	
9	63.2 39	45.2		9	1.9	39	1.7	
10	50.6 40	59.5		10	2.0	40	1.4	
11	71.7 41	35.5		11	1.8	41	1.6	
12	67.1 42	36.8		12	2.1	42	1.8	
13	48.4 43	31.8		13	2.3	43	1.3	
14	28.2 44	12.4		14	2.2	44	1.5	
15	56.2 45	14.2		15	2.4	45	1.3	
16	22.3 46	21.3		16	2.1	46	1.2	
17	26.7 47	28.3		17	2.2	47	1.4	
18	19.4 48	37.8		18	1.8	48	1.3	
19	34.5 49	64.6		19	1.8	49	1.6	5.
20	38.6 50	61.1		20	1.8	50	1.4	
21	47.9 51	44.2		21	2.0	51	1.3	
22	58.3 52	43.3		22	2.3	52	1.3	
23	54.6 53	36.1		23	2.4	53	1.2	A.:
24	50.9 54	33.4		24	2.1	54	1.6	
25	29.4 55	14.4		25	1.8	55	1.3	
26	26.5 56	21.8		26	1.6	56	1.3	THE STATE OF
27	33.4 57	53		27	1.6	57	1.3	** .
28	17.8 58	18		28	1.7	58	1.3	30 C
29	14.2 59	17.2		29	1.7	59	1.9	
30	25.2 60	12.8		30	1.8	60	1.5	
AVG TO	OTAL VOC	35.0	PPM	AVG TO	TAL VOC	;	1.8	PPM
METHA	NE (AS PROP.)	14.5	PPM	METHA	NE (AS P	ROP.)	1.2	PPM
TONBEC	(ACTUAL)	20.5	PPM	TONIMO	(ACTUA	LA.	0.6	PPM
all records a	JRE IN SAMPLE	4.7	%		IRE IN SA	The second second	4.1	%
TGNMC	the first of the second of the	21.5	PPM	TGNMO		user Like	4.7	PPM
TGNMC	(AS CARBON)	32.2	MG/M3	TGNMO	(AS CAR	BON)	1.0	MG/M3
	(AS PROPANE)	39.4	MG/M3	1000	(AS PRO			MG/M3

TGNMO CONCENTRATION-BASED DESTRUCTION EFFICIENCY

96.95 %

VOCS - TEST 2 STACK S10 - DRUM RECLAM FURNACE & AFTERBURNER MID-AMERICA STEEL DRUM - OAK CREEK, WI TABLE 2-5

JUNE 6, 2014

INLET				OUTLET						
TIME	VOC PPM	TIME	VOC PPM	TIME	VOC PPM	TIME	VOC PPM			
1	28.7	31	23.2	1	2.9	31	1.4			
	67.7	32	28.7	2	3.1	32	1.6			
3	97.8	33	30.5	3	3.5	33	1.4	· .		
4	71.0	34	21.3	4	3.1	34	1.5			
2 3 4 5 6	56.4	35	18.1	5	2.8	35	1.8			
6	50.3	36	30.3	6	2.6	36	2.1	="		
7	23.5	37	24.5	7	2.9	37	2.3			
8	27.9	38	22.2	8	2.0	38	1.8			
9	56.6	39	31.8	9	2.1	39	1.5			
10	44.6	40	42.3	10	2.1	40	1.2			
11	38.8	41	52.1	11	2.0	41	1.2			
12	28.1	42	48.1	12	2.3	42	1.1			
13	27.8	43	81.7	13	2.2	43	1.5			
14	29.5	44	83.9	14	2.1	44	1.2			
15	28.7	45	27.8	15	2.1	45	1.0			
16	32.1	46	76.6	16	1.8	46	1.4			
17	20.1	47	78.1	17	1.8	47	1.0	% &		
18	21.8	48	70.6	18	1.8	48	1.0			
19	19.5	49	65.8	19	1.7	49	1.4			
20	49.2	50	75	20	1.8	50	1.1	egen en		
21	30.2	51	57.4	21	1.7	51	1.1	5.5		
22	17.2	52	58.6	22	1.9	52	1.4			
23	21.4	53	54.8	23	1.7	53	1.0			
24	15.4	54	59.6	24	1.6	54	1.6			
25	13.9	55	52.3	25	1.5	55	1.2			
26	22.2	56	56.2	26	1.8	56	1.0			
27	38.3	57	75.4	27	1.8	57	1.1			
28	45.2	58	90.9	28	1.9	58	1.3			
29	45.8	59	86.7	29	1.9	59	1.3			
30 °	53.7	60	83.6	30	1.7	60	1.1			
AVG TO	TAL VOC		45.5 PPM	AVG TO	TAL VOC	•	1.7	PPM		
METHA	NE (AS PF	ROP.)	17.2 PPM	METHA	NE (AS P	ROP.)	1.4	PPM		
TGNMO	(ACTUAL	· · ·	28.3 PPM	TONNO	(ACTUA	14	0.3	PPM		
	RE IN SA		4.7 %		JRE IN SA		4.1	%		
TGNMO			29.7 PPM	TGNMC	100	,,,,,	0.4	PPM		
200	(AS CAR (AS PRO		44.5 MG/M3 54.5 MG/M3		(AS CAR (AS PRO		0.5 0.7	MG/M3 MG/M3		

TGNMO CONCENTRATION-BASED DESTRUCTION EFFICIENCY

98.78 %

VOCS - TEST 3 STACK S10 - DRUM RECLAM FURNACE & AFTERBURNER MID-AMERICA STEEL DRUM - OAK CREEK, WI

TABLE 2-6

JUNE 6, 2014

INLET	- 5				OUTLE	Т			
TIME	VOC PPM	TIME	VOC PPM		TIME	VOC PPM	TIME	VOC PPM	
1	15.4	31	32.4		1	1.0	31	0.3	
2	23.4	32	59.8		2	0.8	32	0.4	
3	32.6	33	62.5		3	0.7	33	0.5	
4	31.8	34	66.3		4	0.6	34	0.3	
5	59.8	35	30.5		5	0.9	35	0.3	
6	48.6	36	22.9		6	0.7	36	0.4	
7	41.8	37	19.5		7	0.8	37	0.6	
8	60.8	38	19.9		8	0.7	38	0.4	
9	63.9	39	20.3		9	0.6	39	0.4	
10	38.2	40	13.5		10	0.7	40	0.3	
11	34.0	41	44		11	0.7	41	0.5	50
12	32.6	42	30.6		12	8.0	42	0.4	
13	36.5	43	42.2		13	0.7	43	0.3	
14	30.2	44	39.9		14	0.6	44	0.3	
15	26.2	45	34.1		15	0.7	45	0.3	
16	20.4	46	20.5		16	0.5	46	0.3	
17	15.9	47	20.6		17	0.5	47	0.3	1 to 1
18	14.3	48	16.3		18	0.5	48	0.7	
19	12.6	49	34		19	0.4	49	0.9	
20	17.4	50	34.1		20	0.4	50	1.2	
21	39.9	51	45.5		21	0.4	51	0.8	
22	42.4	52	36.4		22	0.4	52	0.6	47.00
23	44.1	53	49.3		23	0.4	53	0.5	
24	32.8	54	48.6		24	0.3	54	0.5	
25	36.6	55	60.4		25	0.2	55	1.1	
26	43.8	56	75		26	0.4	56	0.7	
27	50.1	57	50.7		27	0.4	57	0.4	
28	45.8	58	62.2		28	0.4	58	0.4	
29	69.7	59	69.2		29	0.4	59	0.8	
30	73.6	60	62.2		30	0.4	60	0.5	
							*	". *	
AVG TO	TAL VOC	r i	39.3	PPM	AVG TO	TAL VO	3	0.5	PPM
METHA	NE (AS PI	ROP.)	16.1	PPM	METHA	NE (AS P	ROP.)	0.2	PPM
TGNMO	(ACTUAL	_) *	23.2	PPM	TGNMO	(ACTUA	L)	0.3	PPM
4	RE IN SA		4.7	%		JRE IN SA		4.1	%
TGNMO		and the second	24.4	PPM	TGNMO		e a little op 100g	0.4	PPM
200	(AS CAR		36.5	MG/M3		(AS CAF		0.5	MG/M3
TGNMO	(AS PRO	PANE)	44.7	MG/M3	TGNMO	(AS PRO	PANE)	0.7	MG/M3

TGNMO CONCENTRATION-BASED DESTRUCTION EFFICIENCY

98.54 %

3.0 TEST METHODS

3.1 Particulate Matter Testing

The equipment used to sample for particulate matter was the Western Precipitation Division of the Joy Manufacturing Company Emission Parameter Analyzer. Samples were collected and analyzed in accordance with procedures outlined in EPA Method 5 - "Determination of Particulate Emissions from Stationary Sources" as found in 40 CFR Part 60, Appendix A, and EPA Method 202 - "Determination of Condensable Particulate Emissions from Stationary Sources" as found in 40 CFR Part 51, Appendix M.

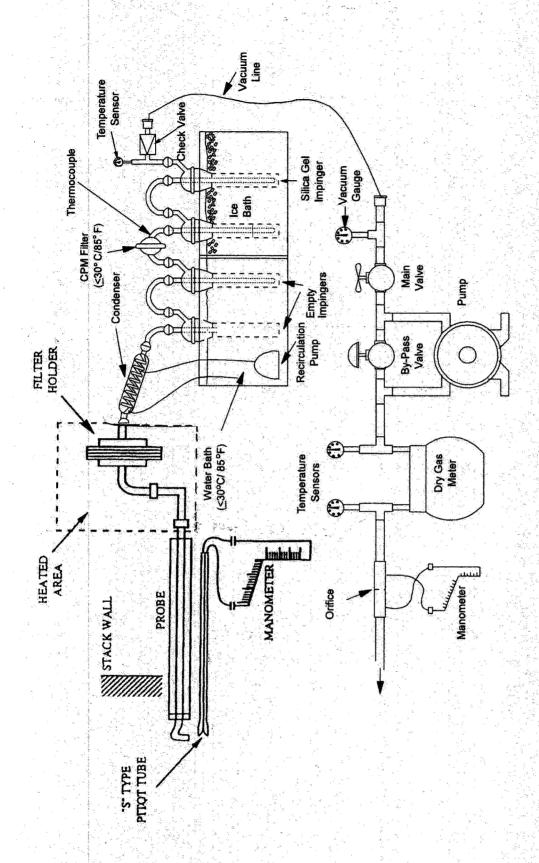
The "front half" of the sampling train consisted of a stainless steel probe tip, a heated stainless steel lined probe, and a heated glass fiber filter (or "filterable particulate" filter). Following the front half, the "back half" of the sampling train consisted of a moisture condenser, several impingers, and a condensable particulate matter (CPM) filter. A schematic drawing of the sampling train is included. The knock-out impinger and second impinger preceding the CPM filter were left dry and were placed in a water bath. The third impinger (immediately following the CPM filter) contained 100 milliliters of deionized water, the fourth was left dry, and the fifth contained a tared amount of silica gel. The gas then passed through a vacuum pump, calibrated dry gas meter, and a calibrated orifice. The temperatures of the stack gas stream, as well as strategic locations within the sampling devices, were monitored by RTDs and read directly from a gauge on the control unit.

The initial gas stream velocity was obtained from a preliminary traverse using an "S" type pitot tube. The initial moisture was estimated from previous tests of similar processes. This data, along with the stack temperature, was used to set a nomograph so that rapid calculations of isokinetic sampling conditions could be made.

The principle of the method was to collect the sample representative of the exhaust by adjusting the sample collection velocity to match the exhaust gas stream velocity at the point of collection. The velocity at the point of collection was measured with an "S" type pitot tube attached to the probe and the collection velocity was matched to the stack gas velocity by adjusting the flow as indicated by the calibrated orifice.

To determine the molecular weight of the stack gas, samples were drawn into an Orsat analyzer and analyzed for percentage CO2, O2, CO, and N2.

At the completion of the test, the probe and tip preceding the filter was washed (rinsed, brushed, and rinsed three times) with acetone. This rinse was later placed in a tared beaker along with a rinse of the filter-holding glassware and evaporated to dryness at room temperature. The filter and beakers were then desiccated to the tared humidity conditions and weighed. These combined weights constituted the filterable (or "front-half") particulate catch.



Schematic of Condensable Particulate Sampling Train

3.1 (continued)

The impinger contents were measured and weighed for determination of the actual moisture content of the exhaust gas stream. Since the stack exhaust was relatively dry, no condensate formed in the knock-out or dry second impinger that preceded the CPM filter. Therefore, no purge of any condensate solution was performed (as noted in EPA Method 202). The condenser, impingers, and connecting glassware which preceded the CPM filter were rinsed with water (twice). The same glassware was then rinsed with acetone and hexane (twice). All rinses were saved for further analysis.

The CPM filter was extracted, with sonication, three times with water and then hexane. The water extractions were added to the impinger (pre CPM filter) condensate catch and rinses; the hexane extractions were added to the acetone/hexane rinses.

The impinger water catch (pre CPM filter) and rinses were then placed into large separatory funnels. An oil/grease type extraction was then performed on the impinger contents using three repeated hexane extractions. The hexane portion from the extractions was added to the previous glassware rinses and was then evaporated off at room temperature leaving any organic residue. The remaining water fraction of the extractions was boiled down to a small volume (approx. 10 ml.) and allowed to dry at room temperature for each sample catch. The remaining residue was then weighed as a measure of any inorganic particulates. The combined weights of the two extraction residues constituted the condensable (or "back-half") particulate fraction.

The combined weights of the filterable and condensable particulate catch were used to determine the total particulate emission rates. Blanks of the sample solutions were also analyzed in similar fashion to the field samples. All test results were blank subtracted as appropriate.

3.2 VOC Test Methods

Testing to determine VOC levels was performed in accordance with the procedures outlined in EPA Method 25A (40 CFR Part 60, Appendix A). Exhaust gas from each of the two sample locations was drawn through a stainless steel probe and a heated Teflon line to an identical on-site FID analyzer (Thermo Environmental Instruments Model 51A). The VOC concentrations of the sampled gas streams could be read directly from the analyzers. Readings were taken every minute and each reading represented the electronically averaged VOC concentration over the previous minute.

The analyzers were calibrated throughout the test efforts using EPA Protocol gas standards (propane in nitrogen). Calibrations were made before and after each test hour. The concentrations of the gas standards used were:

Outlets - 15.1, 25.4, and 45.4 ppm Inlets - 25.4, 45.4, and 86.3 ppm

The certification sheets for the gas standards are included in Appendix B of this report. The calibration gases were introduced into the same sampling train (through the heated line) as the sampled exhaust gas.

3.2 VOC Test Methods (continued)

The VOC readings from the analyzers were corrected (methane levels were subtracted out) for methane levels measured in the exhaust gas streams. Since methane is exempt from the definition of VOCs, this correction was appropriate. The methane levels were determined by gas chromatograph (GC-FID, Chromosorb 102 column) from integrated Tedlar bag samples that were taken during each test period.

4.0 CALIBRATION DATA

The probe tips, pitot tubes, dry gas meters, and sample box orifices used in the test efforts were calibrated prior to the testing in accordance with the procedures outlined in the Maintenance, Calibration, and Operation of Isokinetic Source-Sampling Equipment as published by the US EPA. The values obtained were:

Stack	Stack Date B		Orifice Coeff. (∆H@)	Dry Gas Meter Coeff. (γ)	Probe Tip Diameter	
S10	6/6	2	0.726	1.009	0.188 in. (Test 1), 0.250 in. (Tests 2 & 3)	

The flow measurements were made with an S-type pitot tube attached to the particulate sampling probe. For the sampling probe used, the pitot tube coefficient (C_p) was 0.84. Prior to the first test, the null angles were measured to verify the absence of cyclonic flow. All of the null angles were 5 degrees or less, validating the flow measurements and sampling location.

The dry gas meter installed in the control box was a temperature compensating meter. The correction factor (gamma) for the meter could best be described by the following equations:

Box 2 -
$$\gamma = 1.009 + [(T_M - 70) \times 0.00012]$$

The most recent calibrations on the particulate sampling equipment were performed April 7, 2014.